

Evaluation of Pitzer Ion Interaction Parameters of Aqueous Electrolytes at 25 °C. 1. Single Salt Parameters

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Ion Interaction parameters for 304 single salts in aqueous solution have been obtained for Pitzer's equations. For most of the cases we evaluated, the range of molality extended up to saturation when data were available. The calculated activity coefficients of HCl, LiBr, CaBr₂, Pr(NO₃)₃, and MgSO₄ from our results and Pitzer's were compared to available smoothed experimental data. The comparisons show better agreement with experimental data when we use values of our parameters which were evaluated at higher concentrations than those used by Pitzer.

Introduction

The principal thermodynamic properties of interest for predicting solubilities are activity and osmotic coefficients. The lack of accurate activity coefficients can result in large errors when predicting the solubility in aqueous multicomponent ionic solutions of high ionic strength even when few chemical species are present.

Ionic interaction models provide the simplest and most coherent procedures for calculating the properties of electrolyte components. They use a single set of equations to describe the osmotic and activity coefficients of the components of single salts and mixtures with common ions. An ion interaction model for electrolyte activity coefficients was developed by Pitzer and co-workers (1-4) in the early 1970s. The Pitzer model extended the Debye-Hückel method, using a virial expansion to account for the ionic strength dependence of the short-range forces in binary and ternary ion interactions. The model is applicable to solutions of high ionic strength. Moreover, these equations can be used in iterative calculations since the ion interaction parameters are expressed as explicit functions of ionic strength and need very few parameters to estimate properties of both single and mixed electrolytes. Many publications (5-11) have shown that the Pitzer model results in excellent solubility predictions.

The purpose of this work is to obtain Pitzer ion interaction parameters from osmotic coefficient data on single electrolytes at high concentration, up to nearly saturation. We used a form of the Pitzer ionic interaction model which was developed by Harvie and Weare (5) to predict the solubility of minerals in concentrated mixed salt solutions. The ionic interaction model was fit to published osmotic coefficient data at 25 °C to obtain ion interaction parameters for solution of single salts. The ion interaction parameters from our results are stored on file in a computer as a database, and activity and osmotic coefficients can be calculated simply by identifying the salt and defining the appropriate ionic strength.

General Equations

Recently, Harvie and Weare (5) developed a chemical equilibrium model for calculating mineral solubilities in the Na-K-Mg-Ca-Cl-SO₄-H₂O system at 25 °C. This model was based on the Pitzer equations (1, 2) for aqueous electrolyte solutions. Their equations for calculating the osmotic and mean

ionic activity coefficients for single electrolyte solutions can be written as follows:

$$\phi = 1 + \frac{2}{(m_M + m_X)} \left\{ \frac{-A^\phi I^{3/2}}{1 + bI^{1/2}} + m_M m_X (B_{MX}^\phi + ZC_{MX}) \right\} \quad (1)$$

$$\ln \gamma_{MX} = -|z_M z_X| A^\phi \left[\frac{I^{1/2}}{1 + bI^{1/2}} + \frac{2}{b} \ln (1 + bI^{1/2}) \right] + \\ 4m \left(\frac{\nu_M \nu_X}{\nu} \right) \left(B_{MX} + \frac{I}{2} B'_{MX} \right) + 6m^2 \left(\frac{\nu_M \nu_X}{\nu} \right) \nu_M z_M C_{MX} \quad (2)$$

In eq 1 and 2, m_M is the molality (mol/kg of solvent) of a cation with charge z_M corresponding to stoichiometric coefficient ν_M . Similarly, the subscript X refers to an anion. Also $\nu = \nu_M + \nu_X$ and $I = 1/2 \sum_i m_i z_i^2$ is the ionic strength. The function Z is defined by $Z = \sum_i m_i |z_i| = 2(\sum_M m_M z_M) = 2(\sum_X m_X |z_X|)$ and A^ϕ is the Debye-Hückel coefficient for the osmotic coefficient and is given by

$$A^\phi = \frac{1}{3} \left(\frac{2\pi N_0 d_w}{1000} \right)^{1/2} \left(\frac{e^2}{DkT} \right)^{3/2} \quad (3)$$

where N_0 is Avogadro's number, d_w is the density of water, and D is the static dielectric constant of water at temperature T. Also, k is Boltzmann's constant and e is the electronic charge. The value of A^ϕ at 25 °C is 0.392 and the term b in eq 1 and 2 is an empirical parameter equal to 1.2 at 25 °C (2). The parameters B_{MX}^ϕ , B_{MX} , and B'_{MX} which describe the interaction of pairs of oppositely charged ions represent measurable combinations of the second virial coefficients. They are defined as explicit functions of ionic strength by using the following equations

$$B_{MX}^\phi = \beta_{MX}^{(0)} + \beta_{MX}^{(1)} e^{-\alpha_1 I^{1/2}} + \beta_{MX}^{(2)} e^{-\alpha_2 I^{1/2}} \quad (4)$$

$$B_{MX} = \beta_{MX}^{(0)} + \beta_{MX}^{(1)} f(\alpha_1 I^{1/2}) + \beta_{MX}^{(2)} f(\alpha_2 I^{1/2}) \quad (5)$$

$$B'_{MX} = \beta_{MX}^{(1)} f'(\alpha_1 I^{1/2}) / I + \beta_{MX}^{(2)} f'(\alpha_2 I^{1/2}) / I \quad (6)$$

where

$$f(x) = 2[1 - (1 + x)e^{-x}] / x^2 \quad (7)$$

$$f'(x) = -2[1 - (1 + x + 0.5x^2)e^{-x}] / x^2 \quad (8)$$

For one or both ions in univalent type electrolytes the first two terms of eq 4 and 5 and only the first term of eq 6 are considered where $\alpha_1 = 2$ (2). For higher valence type electrolytes, such as 2-2 electrolytes, the full eq 4, 5, and 6 are used and $\alpha_1 = 1.4$ and $\alpha_2 = 12$ (3).

The single electrolyte third virial coefficients, C_{MX} , account for short-range interaction of ion triplets and are important only at high concentration. They are independent of ionic strength. The parameters C_{MX} and C_{MX}^ϕ , the corresponding coefficients for calculating the osmotic coefficient, are related by (2)

$$C_{MX} = C_{MX}^\phi / (2|z_M z_X|^{1/2}) \quad (9)$$

Table I. Ion Interaction Parameters for 1-1 Electrolytes at 25 °C

compd	$\beta^{(0)}$	$\beta^{(1)}$	C^ϕ	max <i>m</i>	SD	<i>R</i>	ref
HF	0.02212	0.40156	-0.00018	20.000	0.00305	0.9996	12
HCl	0.20332	-0.01668	-0.00372	16.000	0.01443	0.9999	12
HBr	0.24153	-0.16119	-0.00101	11.000	0.02920	0.9994	12
HI	0.23993	0.28351	0.00138	10.000	0.01593	0.9998	12
HClO ₄	0.21617	-0.22769	0.00192	16.000	0.03618	0.9996	12
HNO ₃	0.08830	0.48338	-0.00233	28.000	0.02764	0.9960	12
LiCl	0.20972	-0.34380	-0.00433	19.219	0.05339	0.9982	12
LiBr	0.24554	-0.44244	-0.00293	20.000	0.09391	0.9974	12
LiI	0.14661	0.75394	0.02126	3.000	0.00155	0.9999	12
LiOH	0.05085	-0.07247	-0.00337	5.000	0.00494	0.9959	12
LiClO ₄	0.20400	0.32251	-0.00118	4.500	0.00157	1.0000	12
LiNO ₃	0.13008	0.04957	-0.00382	20.000	0.00639	0.9999	12
LiNO ₂	0.12147	0.45734	-0.00383	19.900	0.01091	0.9997	25
LiClO ₃	0.17049	0.22944	-0.00524	4.200	0.00185	0.999	26
LiBrO ₃	0.08928	0.21573	-0.00005	5.000	0.00096	1.0000	26
LiAc ^a	0.11215	0.20243	-0.00519	4.000	0.00117	0.9999	12
NaF	0.03183	0.18697	-0.00840	1.000	0.00029	0.9999	12
NaCl	0.07722	0.25183	0.00106	6.144	0.00064	1.0000	12
NaBr	0.11077	0.13760	-0.00153	9.000	0.00448	0.9999	12
NaI	0.13463	0.19479	-0.00117	12.000	0.00924	0.9998	12
NaOH	0.17067	-0.08411	-0.00342	29.000	0.08591	0.9950	12
NaClO ₃	0.01908	0.27932	0.00181	3.000	0.00032	0.9999	12
NaClO ₄	0.25446	0.27569	-0.00102	6.000	0.00101	0.9999	12
NaBrO ₃	-0.02154	0.18207	0.00633	2.167	0.00085	0.9973	12
NaNO ₃	0.00388	0.21151	-0.00006	10.830	0.00073	0.9985	41
NaNO ₂	0.04793	0.22465	-0.00226	12.340	0.00639	0.9980	25
NaH ₂ PO ₄	-0.04746	-0.07586	0.00659	6.500	0.00407	0.9910	12
NaH ₂ AsO ₄	-0.07997	0.35866	0.02267	1.300	0.00029	0.9998	12
NaCNS	0.12373	0.08385	-0.00382	18.000	0.02857	0.9973	12
NaBO ₂	-0.05289	-0.10888	0.01497	4.000	0.00218	0.9998	27
NaBF ₄	-0.02603	-0.10084	0.00171	9.000	0.00355	0.9948	27
NaAc ^a	0.13723	0.34195	-0.00474	3.500	0.00096	1.0000	12
KF	0.10013	-0.02175	-0.00159	17.500	0.02093	0.9989	12
KCl	0.04661	0.22341	-0.00044	4.803	0.00036	1.0000	12
KBr	0.05592	0.22094	-0.00162	5.500	0.00036	1.0000	12
KI	0.07253	0.27710	-0.00381	4.500	0.00060	0.9999	12
KOH	0.17501	-0.01634	-0.00267	20.000	0.02650	0.9995	12
KClO ₃	-0.09193	0.23343	0.700	0.00023	0.9999	12	
KBrO ₃	-0.11426	0.20414	0.500	0.00021	0.9999	12	
KNO ₃	-0.08511	0.10518	0.00773	3.500	0.00042	1.0000	12
KNO ₂	0.00349	0.15708	-0.00025	34.120	0.01196	0.9776	25
KH ₂ PO ₄	-0.11411	0.06898	0.02069	1.800	0.00024	1.0000	12
KH ₂ AsO ₄	-0.12614	0.25457	0.04002	1.300	0.00027	0.9999	12
KCNS	0.03891	0.25361	-0.00192	5.000	0.00062	0.9999	12
KPF ₆	-0.13710	-0.42785	0.500	0.00143	0.9996	12	
KAc ^a	0.15283	0.35513	-0.00432	3.500	0.00087	1.0000	12
RbF	0.10872	0.39804	-0.00874	3.500	0.00191	0.9998	12
RbCl	0.04660	0.12983	-0.00163	7.800	0.00129	0.9999	12
RbBr	0.03868	0.16723	-0.00123	5.000	0.00048	0.9999	12
RbI	0.03902	0.15224	-0.00095	5.000	0.00035	1.0000	12
RbNO ₃	-0.08174	-0.03175	0.00624	4.500	0.00226	0.9996	12
RbNO ₂	-0.00303	0.05130	-0.00014	62.300	0.01944	0.9736	25
RbAc ^a	0.16296	0.32918	-0.00561	3.500	0.00062	1.0000	12
CsF	0.13644	0.14166	-0.00674	3.500	0.00169	0.9999	12
CsCl	0.03643	-0.01169	-0.00096	11.000	0.00365	0.9993	12
CsBr	0.02311	0.04587	0.00092	5.000	0.00141	0.9995	12
CsI	0.02121	0.07307	-0.00307	3.000	0.00038	0.9997	12
CsNO ₃	-0.13004	0.08169	0.03018	1.500	0.00057	0.9999	12
CsNO ₂	0.00926	0.32052	-0.00036	36.000	0.01796	0.9330	25
CsOH	0.14768	0.34572	-0.00819	1.200	0.00037	1.0000	12
CsAc ^a	0.17144	0.32896	-0.00793	3.500	0.00063	1.0000	12
AgNO ₃	-0.07102	-0.16793	0.00322	13.000	0.00823	0.9984	12
TICl	-3.16406	-2.43821	0.010	0.00024	0.9996	12	
TICIO ₄	-0.11111	0.07553	0.500	0.00039	0.9999	12	
TINO ₃	-0.12518	-0.30145	0.400	0.00037	0.9999	12	
TINO ₂	-0.65041	-0.11038	0.37782	1.400	0.00026	1.0000	12
TlAc ^a	0.00878	-0.04105	-0.00153	6.000	0.00215	0.8848	12
NH ₄ Cl	0.05191	0.17937	-0.00301	7.405	0.00093	0.9999	12
NH ₄ I	0.05701	0.31566	-0.00308	7.500	0.00174	0.9998	28
NH ₄ ClO ₄	-0.00697	-0.05618	-0.00071	2.100	0.00024	0.9995	12
NH ₄ NO ₃	-0.01476	0.13826	0.00029	25.954	0.00538	0.9977	12
NH ₄ SCN	0.00528	-0.34080	-0.00036	23.431	0.00490	0.9822	29
Et ₄ NNO ₃	-0.04022	-0.87108	0.00565	8.000	0.00758	0.9893	28
Me ₄ NNO ₃	0.01224	-0.32933	0.00090	7.000	0.00212	0.9991	28
MeNH ₃ ClO ₄	-0.03371	0.00573	0.00345	4.000	0.00168	0.9980	30
Me ₂ NH ₂ ClO ₄	-0.04395	-0.17191	0.00240	7.500	0.00112	0.9999	30
Me ₃ NHClO ₄	-0.11447	-0.17129	0.01348	1.800	0.00235	0.9992	30

Table I (Continued)

compd	$\beta^{(0)}$	$\beta^{(1)}$	C^ϕ	max m	SD	R	ref
GuCl	-0.02855	-0.10997	0.00177	12.000	0.00677	0.9845	31
Li <i>p</i> -tol ^b	0.01223	0.46653	0.00633	4.500	0.00302	0.9986	12
Na <i>p</i> -tol ^b	-0.03958	0.47846	0.00571	4.000	0.00252	0.9951	12
Na form ^c	0.07187	0.32247	-0.00236	3.500	0.00059	0.9999	12
Na propion ^d	0.18813	0.26772	-0.01288	3.000	0.00046	1.0000	12
Na butyr ^e	0.26081	0.16368	-0.03358	3.500	0.00373	0.9998	12
Na valer ^f	0.33473	-0.11324	-0.07394	2.000	0.00295	0.9998	12
Na capryl ^g	-0.45120	-7.73638	0.05902	3.000	0.01695	0.9963	12
Na pelargon ^h	0.03728	-10.3798	-0.07164	2.500	0.01685	0.9933	12
Na capr ⁱ	0.07992	-7.40138	-0.06028	1.800	0.00330	0.9987	12
NaH malon ^j	0.02166	0.17611	-0.00089	5.000	0.00053	0.9998	12
NaH succ ^k	0.03463	0.14036	0.00061	5.000	0.00204	0.9994	12
NaH adip ^l	0.04325	0.33988	0.700	0.00030	0.9999	12	
K <i>p</i> -tol ^b	-0.09842	0.47188	0.01182	3.500	0.00204	0.9995	12
KH malon	-0.00474	0.06128	0.00048	5.000	0.00274	0.8707	12
KH succ	0.01309	0.10978	0.00215	4.500	0.00235	0.9972	12
KH adip	-0.03998	0.47595	0.05523	1.000	0.00070	0.9997	12

^aAcetate. ^b*p*-Toluenesulfonate. ^cFormate. ^dPropionate. ^eButyrate. ^fValerate. ^gCaprylate. ^hPelargonate. ⁱCaprate. ^jMalonate. ^kSuccinate. ^lAdipate.

Table II. Ion Interaction Parameters for 1-2 Electrolytes at 25 °C

compd	$\beta^{(0)}$	$\beta^{(1)}$	C^ϕ	max m	SD	R	ref
H ₂ SO ₄	0.14098	-0.56843	-0.00237	27.500	0.04874	0.9984	32
Li ₂ SO ₄	0.14473	1.29952	-0.00616	3.000	0.00448	0.9996	13
Li ₂ C ₉ H ₄ S ₂ O ₆	0.40862	1.92482	-0.03240	2.500	0.00311	0.9999	13
Li ₂ C ₁₄ H ₁₂ S ₂ O ₆	0.12189	1.48771	0.03415	1.000	0.00395	0.9992	13
Na ₂ SO ₄	0.04604	0.93350	-0.00483	1.750	0.00112	0.9996	13
Na ₂ SO ₃	0.08015	1.18500	-0.00436	2.000	0.00187	0.9996	13
Na ₂ CO ₃	0.05306	1.29262	0.00094	2.750	0.00257	0.9993	13
Na ₂ HPO ₄	-0.02169	1.24472	0.00726	2.000	0.00052	0.9997	13
Na ₂ CrO ₄	0.06526	1.63256	0.00884	4.250	0.00512	0.9997	13
Na ₂ S ₂ O ₃	0.06347	1.32115	0.00475	4.000	0.00335	0.9997	13
Na ₂ S ₂ O ₆	0.08526	1.18961	0.800	0.00271	0.9986	13	
Na ₂ S ₂ O ₈	0.28075	1.01750	0.090	0.00045	0.9999	13	
Na ₂ C ₂ H ₄ S ₂ O ₆	0.28782	1.31451	-0.04835	1.750	0.00518	0.9994	13
Na ₂ C ₆ H ₄ S ₂ O ₆	0.25277	2.02265	-0.02132	3.000	0.00240	0.9999	13
Na ₂ C ₁₄ H ₁₂ S ₂ O ₆	0.00808	1.60199	0.400	0.00427	0.9926	13	
Na ₂ C ₁₄ H ₁₂ S ₂ O ₈	-0.36838	0.16958	0.400	0.00983	0.9817	13	
Na ₂ B ₁₂ H ₁₂	0.51666	1.76589	-0.01834	1.500	0.00091	1.0000	13
Na ₂ WO ₄	0.20318	0.87616	-0.01941	2.500	0.00283	0.9999	13
Na ₂ HAsO ₄	0.13607	1.70125	0.01202	1.000	0.00058	0.9999	13
Na ₂ C ₄ H ₂ O ₄ ^a	0.23506	0.87329	-0.02155	2.000	0.00390	0.9997	13
Na ₂ C ₄ H ₂ O ₄ ^b	0.14005	0.45288	-0.00911	2.750	0.00254	0.9998	13
K ₂ SO ₄	0.07548	0.44371	0.692	0.00136	0.9990	13	
K ₂ HPO ₄	0.05307	1.10271	0.800	0.00049	0.9999	13	
K ₂ H ₂ P ₂ O ₇	-0.00585	1.25198	0.00524	3.000	0.00084	0.9995	13
K ₂ HAsO ₄	0.10670	1.71714	0.800	0.00143	0.9998	13	
K ₂ CrO ₄	0.07702	1.22681	-0.00095	3.250	0.00274	0.9997	13
K ₂ Cr ₂ O ₇	-0.01111	2.33306	0.507	0.01552	0.9144	13	
K ₂ Pt(CN) ₄	0.05955	2.25539	0.948	0.00420	0.9984	13	
Rb ₂ SO ₄	0.09123	0.77863	-0.01282	1.500	0.00097	0.9999	13
Rb ₂ S ₂ O ₈	0.20464	-0.26340	0.070	0.00005	0.9999	13	
Cs ₂ SO ₄	0.14174	0.69456	-0.02686	1.831	0.00113	0.9999	13
Cs ₂ S ₂ O ₈	0.13283	-0.76429	0.109	0.00006	0.9999	13	
(NH ₄) ₂ SO ₄	0.04841	1.13240	-0.00155	5.500	0.00185	0.9996	22
(NH ₄) ₂ HPO ₄	-0.0425.	-0.69871	0.00527	3.000	0.00155	0.9990	13
(NH ₄) ₂ B ₁₀ H ₁₀	0.15824	1.46202	-0.01710	3.750	0.00675	0.9988	13
(CN ₃ H ₆) ₂ CO ₃	-0.07420	0.22809	0.01380	2.500	0.00211	0.9983	13
C ₆ H ₆ S ₂ O ₆	0.42897	2.00694	-0.01984	5.500	0.00782	0.9999	13
C ₆ H ₆ S ₂ O ₆	0.41381	2.01836	-0.02071	1.750	0.00208	0.9999	13

^aSodium fumarate. ^bSodium maleate.

Evaluation of Ion Interaction Parameters

The ion interaction parameters for single electrolytes were evaluated from recently published osmotic coefficient data by using multiple regression analysis to fit eq 1 to the data at 25 °C. We used the computer program SIPS (Statistical Interactive Programming System), which was developed at Oregon State University, for this purpose. The best values of these fitting

parameters are given in Tables I-VI. Tables I-VI also contain the maximum molality for which data are available, frequently up to saturation. Thus the maximum molalities for most cases in our evaluation go beyond that of Pitzer's evaluation (2).

The standard deviation of fit (SD) for the osmotic coefficient data and the multiple correlation coefficient, R, which is a measure of the closeness of fit to a linear relationship, are also listed in Tables I-VI. The source of the osmotic coefficient data is listed in the last column in the tables.

Table III. Ion Interaction Parameters for 2-1 Electrolytes at 25 °C

compd	$\beta^{(0)}$	$\beta^{(1)}$	C^ϕ	max m	SD	R	ref
MgCl ₂	0.35573	1.61738	0.00474	5.750	0.00360	1.0000	14
MgBr ₂	0.4346	1.73184	0.00275	5.610	0.00585	1.0000	14
MgI ₂	0.49161	1.78273	0.00780	5.000	0.00421	1.0000	14
Mg(ClO ₄) ₂	0.49753	1.79492	0.00875	4.000	0.00661	0.9999	22
Mg(NO ₃) ₂	0.34284	2.68244	-0.00723	5.000	0.00760	0.9999	22
Mg(Ac) ₂	0.22930	2.04167	-0.01460	4.000	0.00370	0.9999	22
CaCl ₂	0.32579	1.38412	-0.00174	6.000	0.01582	0.9998	14
CaBr ₂	0.33899	2.04551	0.01067	6.000	0.00715	1.0000	14
CaI ₂	0.43225	1.84879	0.00085	1.915	0.00162	1.0000	14
Ca(ClO ₄) ₂	0.47924	2.16287	-0.00837	6.000	0.01730	0.9999	22
Ca(NO ₃) ₂	0.17030	2.02106	-0.00690	6.000	0.01346	0.9987	22
SrCl ₂	0.28170	1.61666	-0.00071	3.500	0.00392	0.9999	14
SrBr ₂	0.32410	1.78223	0.00344	2.100	0.00086	1.0000	14
SrI ₂	0.39394	1.92536	0.00474	1.970	0.00089	1.0000	14
Sr(ClO ₄) ₂	0.44138	2.00236	-0.01454	6.000	0.00641	0.9999	22
Sr(NO ₃) ₂	0.11832	2.41503	-0.00852	4.000	0.00594	0.9970	22
BaCl ₂	0.29073	1.24998	-0.03046	1.785	0.00147	0.9999	14
BaBr ₂	0.31552	1.57056	-0.01610	2.300	0.00269	0.9999	14
BaI ₂	0.40227	1.90862	-0.00936	1.998	0.00175	1.0000	14
Ba(ClO ₄) ₂	0.32673	2.53859	-0.01576	5.500	0.01015	0.9998	22
Ba(NO ₃) ₂	-0.04371	1.11778		0.400	0.00138	0.9815	22
Ba(Ac) ₂	0.28725	2.87507	-0.04539	3.500	0.00663	0.9994	22
MnCl ₂	0.29486	2.01251	-0.01528	7.500	0.02434	0.9990	16
MnBr ₂	0.44655	1.34477	-0.02269	5.640	0.00546	0.9999	16
Mn(ClO ₄) ₂	0.50957	2.16209	0.01144	3.456	0.00324	1.0000	16
NiCl ₂	0.39304	0.99773	-0.01658	5.500	0.01386	0.9998	15
NiBr ₂	0.44305	1.48323	-0.00590	4.500	0.00866	0.9999	15
Ni(ClO ₄) ₂	0.49285	1.98517	0.01679	3.500	0.00237	1.0000	15
Ni(NO ₃) ₂	0.30978	2.10644	-0.00394	4.500	0.01024	0.9999	15
CoCl ₂	0.37351	1.25999	-0.01803	4.000	0.00711	0.9999	15
CoBr ₂	0.47172	0.98425	-0.01716	5.750	0.02159	0.9997	15
CoI ₂	0.51953	1.71266	-0.00101	4.000	0.01570	0.9999	15
Co(NO ₃) ₂	0.30654	1.80197	-0.00649	5.500	0.00491	0.9999	15
Co(ClO ₄) ₂	0.50409	1.96664	0.01349	3.500	0.00325	1.0000	15
CuCl ₂	0.23052	2.20897	-0.01639	5.750	0.00664	0.9976	16
CuBr ₂	0.41247	1.66270	-0.04262	3.606	0.00586	0.9999	16
Cu(ClO ₄) ₂	0.48984	1.90361	0.00839	3.500	0.00173	1.0000	16
Cu(NO ₃) ₂	0.28124	1.72906	-0.00842	7.840	0.00307	1.0000	16
Cu(C ₇ H ₇ O ₃ S) ₂	0.08473	1.79523		0.800	0.00207	0.9995	16
FeCl ₂	0.35011	1.40092	-0.01412	2.000	0.00182	1.0000	15
ZnF ₂	0.00144	-0.08746		0.142	0.00057	0.9327	17
ZnCl ₂	0.08887	2.94869	0.00095	10.000	0.01442	0.9995	17
ZnBr ₂	0.18728	4.34674	-0.00911	6.000	0.04579	0.9888	17
ZnI ₂	0.28596	5.08037	-0.02004	6.000	0.07265	0.9813	17
Zn(ClO ₄) ₂	0.52365	1.46569	0.00748	4.300	0.01012	0.9999	17
Zn(NO ₃) ₂	0.32587	1.90781	-0.00842	6.750	0.00283	1.0000	17
Zn(C ₇ H ₇ O ₃ S) ₂	0.11840	1.67138		0.300	0.00037	0.9999	17
CdCl ₂	0.01624	0.43945	0.00109	6.000	0.00108	0.9998	22
CdBr ₂	0.02087	-0.86302	0.00284	4.000	0.00370	0.9989	22
CdI ₂	0.14916	0.55935	-0.01117	2.500	0.00341	0.9995	22
Cd(ClO ₄) ₂	0.38986	1.99610	0.02075	1.750	0.00117	1.0000	17
Cd(NO ₂) ₂	0.00265	-2.15854	0.00302	7.840	0.01903	0.9917	17
Cd(NO ₃) ₂	0.28764	1.68468	-0.02587	2.500	0.00318	0.9999	17
Cd(C ₇ H ₇ O ₃ S) ₂	0.07161	1.75817		0.600	0.00286	0.9999	17
PbCl ₂	0.08010	-2.57126		0.039	0.00375	0.9833	16
Pb(ClO ₄) ₂	0.33500	1.61813	-0.00904	10.830	0.00461	1.0000	16
Pb(NO ₃) ₂	0.01506	-0.27095	-0.01330	1.830	0.00479	0.9410	16
UO ₂ Cl ₂	0.040951	1.74913	-0.02949	3.174	0.00538	0.9999	16
UO ₂ (ClO ₄) ₂	0.66563	1.42853	0.00699	4.000	0.01302	0.9999	16
UO ₂ (NO ₃) ₂	0.47803	1.59530	-0.03971	5.500	0.01444	0.9997	16
C ₈ H ₂₂ N ₂ Cl ₂	0.10390	-0.10568	0.00165	4.400	0.00452	0.9998	17
C ₈ H ₂₂ N ₂ I ₂	-0.07160	-0.85778	0.01156	4.000	0.00941	0.9792	17
[Co(NH ₃) ₅ NO ₂]Cl ₂	-2.71103	6.03902		0.100	0.00324	0.9958	15
[Co(NH ₃) ₅ Cl]Cl ₂	1.44407	0.63074		0.008	0.00031	0.9991	15
[Co(NH ₃) ₅ F]Cl ₂	0.03945	0.64984	-0.00976	1.000	0.00037	0.9999	15
[Co(NH ₃) ₅ Cl](ClO ₄) ₂	0.03550	0.61167		0.100	0.00155	0.9914	15
[Co(NH ₃) ₅ CH ₃ CH ₂ COO](NO ₃) ₂	-0.01298	0.46747		0.400	0.00084	0.9950	15
[Co(NH ₃) ₅ CH ₃ CH ₂ COO]I ₂	0.02342	0.55520		0.500	0.00297	0.9833	15
[Co(NH ₃) ₅ CH ₃ CH ₂ COO]Br ₂	0.05240	0.48711	-0.00539	1.200	0.00062	0.9998	15
[Co(NH ₃) ₅ CH ₃ CH ₂ COO]Cl ₂	0.11194	0.34489	-0.01339	2.400	0.00187	0.9997	15
[Co(NH ₃) ₅ CH ₃ COO](NO ₃) ₂	0.38956	-0.41144		0.050	0.00009	0.9998	15
[Co(NH ₃) ₅ CH ₃ COO]I ₂	0.40728	-0.31106		0.100	0.00042	0.9996	15
[Co(NH ₃) ₅ CH ₃ COO]Br ₂	0.04621	0.52415		0.600	0.00115	0.9986	15
[Co(NH ₃) ₅ CH ₃ COO]Cl ₂	0.07197	0.39910		0.600	0.00422	0.9857	15
[Co(NH ₃) ₅ (CH ₃) ₂ CHCOO](NO ₃) ₂	-0.01831	0.35251	0.00279	2.500	0.00201	0.9844	15
[Co(NH ₃) ₅ (CH ₃) ₂ CHCOO]I ₂	0.00203	0.58539		0.800	0.00252	0.9832	15
[Co(NH ₃) ₅ (CH ₃) ₂ CHCOO]Br ₂	0.05108	0.36726		0.800	0.00369	0.9880	15

Table III (Continued)

compd	$\beta^{(0)}$	$\beta^{(1)}$	C^ϕ	max <i>m</i>	SD	<i>R</i>	ref
[Co(NH ₃) ₅ (CH ₃) ₂ CHCOO]Cl ₂	0.109 66	0.351 57	-0.012 93	2.500	0.002 01	0.9997	15
cis-[Co(C ₂ H ₈ N ₂)NH ₃ NO ₂](NO ₃) ₂	-0.075 13	0.395 44		0.600	0.000 70	0.9983	15
cis-[Co(C ₂ H ₈ N ₂)NH ₃ NO ₂]I ₂	-0.138 44	0.645 45		0.600	0.002 49	0.9941	15
cis-[Co(C ₂ H ₈ N ₂)NH ₃ NO ₂]Br ₂	-0.114 89	0.368 41	0.034 49	1.000	0.002 11	0.9970	15
cis-[Co(C ₂ H ₈ N ₂)NH ₃ NO ₂]Cl ₂	-0.012 70	0.571 58	0.007 24	2.800	0.001 57	0.9957	15
trans-[Co(C ₂ H ₈ N ₂)NH ₃ NO ₂](NO ₃) ₂	-0.064 65	0.317 15		0.800	0.001 12	0.9978	15
trans-[Co(C ₂ H ₈ N ₂)NH ₃ NO ₂]I ₂	-0.176 04	1.096 89		0.300	0.001 77	0.9852	15
trans-[Co(C ₂ H ₈ N ₂)NH ₃ NO ₂]Br ₂	-0.058 42	0.393 91	0.013 33	2.400	0.000 83	0.9993	15
trans-[Co(C ₂ H ₈ N ₂)NH ₃ NO ₂]Cl ₂	0.014 21	0.590 51	0.004 82	2.400	0.000 84	0.9997	15

Table IV. Ion Interaction Parameters for 3-1, 1-3 Electrolytes at 25 °C

compd	$\beta^{(0)}$	$\beta^{(1)}$	C^ϕ	max <i>m</i>	SD	<i>R</i>	ref
LaCl ₃	0.596 02	5.6000	-0.024 64	3.800	0.0083	0.9999	18
La(ClO ₄) ₃	0.838 15	6.5333	-0.012 88	4.500	0.0269	0.9998	33
La(NO ₃) ₃	0.305 07	5.1333	-0.017 50	4.000	0.0314	0.9963	21
La(C ₂ H ₅ SO ₄) ₃	0.805 06	5.2315	-0.103 89	1.100	0.0003	1.0000	34
PrCl ₃	0.588 04	5.6000	-0.020 60	3.800	0.0108	0.9999	18
Pr(ClO ₄) ₃	0.824 54	6.5333	-0.009 14	4.500	0.0240	0.9999	33
Pr(NO ₃) ₃	0.326 15	5.1333	-0.018 51	4.000	0.0290	0.9973	21
Pr(C ₂ H ₅ SO ₄) ₃	0.809 96	5.3111	-0.099 72	0.800	0.0003	1.0000	34
NdCl ₃	0.586 74	5.6000	-0.018 82	3.800	0.0102	0.9999	18
Nd(ClO ₄) ₃	0.814 68	6.5333	-0.006 77	4.500	0.0209	0.9999	33
Nd(NO ₃) ₃	0.339 27	5.1333	-0.019 45	4.000	0.0277	0.9977	21
Nd(C ₂ H ₅ SO ₄) ₃	0.791 01	5.4928	-0.091 35	1.100	0.0003	1.0000	34
SmCl ₃	0.593 61	5.6000	-0.019 14	3.600	0.0095	0.9999	18
Sm(ClO ₄) ₃	0.826 73	6.5333	-0.004 87	4.500	0.0211	0.9999	33
Sm(NO ₃) ₃	0.358 02	5.1333	-0.018 84	4.200	0.0235	0.9987	20
Sm(C ₂ H ₅ SO ₄) ₃	0.844 86	5.8016	-0.100 39	0.800	0.0002	1.0000	34
EuCl ₃	0.601 35	5.6000	-0.019 26	3.400	0.0089	0.9999	18
Eu(C ₂ H ₅ SO ₄) ₃	0.801 48	5.6723	-0.086 13	1.100	0.0003	1.0000	34
Ga(ClO ₄) ₃	0.785 35	5.2055	0.042 02	2.000	0.0072	0.9999	22
GdCl ₃	0.611 42	5.6000	-0.019 24	3.400	0.0084	0.9999	18
Gd(ClO ₄) ₃	0.848 32	6.5333	-0.007 92	4.500	0.0197	0.9999	33
Gd(NO ₃) ₃	0.378 41	5.1333	-0.019 60	4.200	0.0283	0.9986	20
Gd(C ₂ H ₅ SO ₄) ₃	0.851 52	5.4619	-0.102 24	0.800	0.0004	1.0000	34
TbCl ₃	0.622 31	5.6000	-0.019 23	3.400	0.0088	0.9999	18
Tb(ClO ₄) ₃	0.883 29	6.5333	-0.011 12	4.600	0.0290	0.9998	19
Tb(NO ₃) ₃	0.368 50	5.1333	-0.017 94	4.400	0.0291	0.9983	20
Tb(C ₂ H ₅ SO ₄) ₃	0.849 99	5.6688	-0.096 76	1.100	0.0004	1.0000	34
DyCl ₃	0.628 26	5.6000	-0.018 95	3.600	0.0108	0.9999	18
Dy(ClO ₄) ₃	0.880 21	6.5333	-0.009 47	4.500	0.0297	0.9998	33
Dy(C ₂ H ₅ SO ₄) ₃	0.851 38	5.9023	-0.092 48	1.100	0.0003	1.0000	34
HoCl ₃	0.623 46	5.6000	-0.016 75	3.600	0.0111	0.9999	18
Ho(ClO ₄) ₃	0.871 29	6.5333	-0.006 99	4.500	0.0346	0.9998	33
Ho(C ₂ H ₅ SO ₄) ₃	0.843 17	5.4972	-0.093 96	1.100	0.0003	1.0000	34
ErCl ₃	0.621 58	5.6000	-0.015 24	3.600	0.0109	0.9999	18
Er(ClO ₄) ₃	0.875 06	6.5333	-0.006 71	4.500	0.0348	0.9998	33
Er(NO ₃) ₃	0.431 14	5.1333	-0.025 87	4.000	0.0289	0.9983	20
Er(C ₂ H ₅ SO ₄) ₃	0.853 45	5.6291	-0.093 71	1.100	0.0004	1.0000	34
TmCl ₃	0.626 40	5.6000	-0.015 13	3.800	0.0120	0.9999	18
Tm(ClO ₄) ₃	0.875 13	6.5333	-0.006 17	4.500	0.0342	0.9998	33
Tm(NO ₃) ₃	0.453 94	5.1333	-0.027 76	4.000	0.0277	0.9986	20
Tm(C ₂ H ₅ SO ₄) ₃	0.845 89	5.6167	-0.092 79	1.100	0.0003	1.0000	oj
YbCl ₃	0.625 80	5.6000	-0.014 53	4.000	0.0120	0.9999	18
Yb(ClO ₄) ₃	0.881 16	6.5333	-0.006 64	4.500	0.0315	0.9998	33
Yb(NO ₃) ₃	0.467 44	5.1333	-0.028 12	4.000	0.0242	0.9990	20
Yb(C ₂ H ₅ SO ₄) ₃	0.859 15	5.6640	-0.090 78	1.200	0.0002	1.0000	34
LuCl ₃	0.621 06	5.6000	-0.013 56	4.000	0.0113	0.9999	18
Lu(ClO ₄) ₃	0.868 83	6.5333	-0.001 88	4.000	0.0291	0.9998	33
Lu(C ₂ H ₅ SO ₄) ₃	0.862 56	5.7210	-0.091 67	1.200	0.0003	1.0000	34
AlCl ₃	0.686 27	6.0203	0.008 10	1.800	0.0088	0.9999	22
ScCl ₃	0.720 87	6.5317	0.033 67	1.800	0.0044	0.9999	22
CrCl ₃	0.690 81	2.7849	-0.043 90	1.200	0.0033	0.9999	22
Cr(NO ₃) ₃	0.724 90	6.3169	-0.059 93	1.400	0.0035	0.9999	22
YCl ₃	0.625 70	5.6000	-0.015 71	3.800	0.0117	0.9999	18
Y(C ₂ H ₅ SO ₄) ₃	0.851 87	5.6577	-0.093 22	1.200	0.0003	1.0000	34
CeCl ₃	0.635 09	7.4991	-0.030 01	2.000	0.0127	0.9996	22
FeCl ₃	0.236 17	-5.3975	-0.007 96	10.000	0.0087	0.9999	35
Na ₃ PO ₄	0.135 14	5.4136		0.700	0.0063	0.9401	22
Na ₃ AsO ₄	0.201 93	5.5366		0.700	0.0048	0.9932	22
K ₃ PO ₄	0.316 68	7.4659		0.700	0.0079	0.9942	22
K ₃ AsO ₄	0.422 91	9.9809		0.011	0.0111	0.9934	22
K ₃ Fe(cn) ₆	0.349 15	5.5849	-0.045 08	1.400	0.0034	0.9995	22
K ₃ Co(cn) ₆	0.365 92	1.6190	-0.069 46	1.311	0.0247	0.9890	36
Co(en) ₃ Cl ₃	0.185 92	3.8000	-0.027 83	1.000	0.0009	0.9997	22
Co(en) ₃ (NO ₃) ₃	0.103 40	3.5513		0.275	0.0013	0.9997	36
Co(pn) ₃ (ClO ₄) ₃	0.148 54	2.9504		0.261	0.0036	0.9973	36

Table V. Ion Interaction Parameters for 4-1, 1-4 Electrolytes at 25 °C

compd	$\beta^{(0)}$	$\beta^{(1)}$	C^ϕ	max <i>m</i>	SD	<i>R</i>	ref
K ₄ Mo(CN) ₈	0.00575	-7.4744	0.01015	1.400	0.0132	0.9878	22
K ₄ Fe(CN) ₆	-0.00638	-10.6019		0.900	0.0155	0.9799	22
K ₄ P ₂ O ₇	0.05939	-9.2939	0.01591	2.300	0.0099	0.9989	37
K ₄ W(CN) ₈	0.38299	6.1624	-0.05810	1.500	0.0192	0.9948	38
K ₄ ATP ^a	0.08619	-4.8045	0.01494	2.400	0.0080	0.9994	39
Na ₄ ATP ^a	-0.04154	-6.0631	0.03044	2.000	0.0093	0.9974	39
Na ₄ P ₂ O ₇	0.06250	-11.1364		0.230	0.0038	0.9929	37
ThCl ₄	0.47146	-9.4843	-0.00078	1.800	0.0179	0.9994	22
Th(NO ₃) ₄	0.35392	-7.6453	-0.01869	5.000	0.0126	0.9997	22
Pt(pn) ₃ Cl ₄	0.28756	10.7131		0.100	0.0063	0.9983	38
[N(Me) ₄] ₄ Mo(CN) ₈	0.53495	9.6607	0.08620	1.440	0.0120	0.9988	38

^a ATP = adenosine 5'-triphosphate.

Table VI. Ion Interaction Parameters for 2-2 Electrolytes at 25 °C

compd	$\beta^{(0)}$	$\beta^{(1)}$	$\beta^{(2)}$	C^ϕ	max <i>m</i>	SD	<i>R</i>	ref
CuSO ₄	0.20458	2.7490	-42.038	0.01886	1.400	0.00175	0.9999	22, 23
ZnSO ₄	0.18404	3.0310	-27.709	0.03286	3.500	0.00212	1.0000	22, 23
CdSO ₄	0.20948	2.6474	-44.473	0.01021	3.500	0.00265	0.9999	22, 23
NiSO ₄	0.15471	3.0769	-37.593	0.04301	2.500	0.00310	0.9999	22, 23
MgSO ₄	0.22438	3.3067	-40.493	0.02512	3.000	0.00346	0.9999	22, 23
MnSO ₄	0.20563	2.9362	-38.931	0.01650	4.000	0.00470	0.9999	22, 23
BeSO ₄	0.31982	3.0540	-77.689	0.00598	4.000	0.00421	0.9999	22, 23
UO ₂ SO ₄	0.33190	2.4208	98.958	-0.01789	6.000	0.00224	1.0000	22
CaSO ₄	0.20000	3.7762	-58.388		0.020	0.00460	0.9863	23
CoSO ₄	0.20000	2.9709	-28.752		0.100	0.00248	0.9992	23

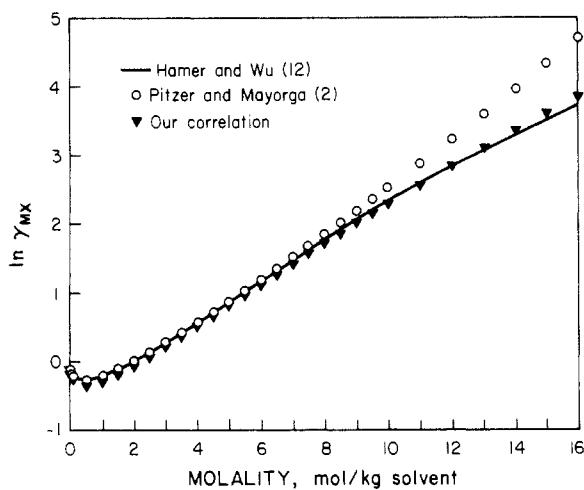


Figure 1. Comparison of experimental smoothed γ_{MX} with values calculated from Pitzer and present work for HCl at 25 °C.

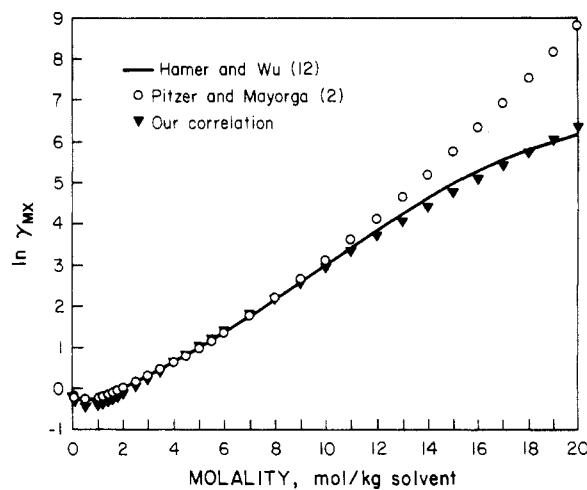


Figure 2. Comparison of experimental smoothed γ_{MX} with values calculated from Pitzer and present work for LiBr at 25 °C.

In most cases where one or both ions are univalent, we used the experimental osmotic coefficient data evaluated by Hamer and Wu (12) for 1-1 electrolytes, Goldberg (13) for 1-2 electrolytes, Goldberg and Nuttall (14-17) for 2-1 electrolytes, and Spedding et al. (18-21) for 3-1 electrolytes.

For 2-2 type electrolytes, we used osmotic coefficient data from Robinson and Stokes (22) and Pitzer (23) who provided the data below 0.1 *m*, except for UO₂SO₄. Data for UO₂SO₄ are available only over concentration range of 0.1-0.6 *m*.

The positive value of the coefficients B_{MX}^ϕ from eq 4 indicates the net predominance of repulsive short-range interaction forces according to Pitzer and Mayorga (2).

For pure electrolytes, the two ion interaction parameters, $\beta_{MX}^{(0)}$ and $\beta_{MX}^{(1)}$, define the second virial coefficients which describe the interaction of pairs of oppositely charged ions. However, for 2-2 and higher valence electrolytes, one additional term, $\beta_{MX}^{(2)}$, which reproduces the irregular behavior in the range below 0.1 *m*, is added (3). From eq 5 and 6, one finds that the $\beta_{MX}^{(2)}$ term is equal to 0.00005 $\beta_{MX}^{(0)}$ at 0.1 *m* and negligible above 0.1 *m* because of the large value of $\alpha_2 = 12.0$. For the case of

UO₂SO₄, there are no osmotic coefficient data below 0.1 *m*; hence the $\beta_{MX}^{(2)}$ value does not affect the relative values of osmotic and activity coefficients in the given concentration range and has no meaningful value. In the cases of CaSO₄ and CoSO₄, where available data are limited to dilute solutions (below 0.1 *m*), we omitted the coefficients C_{MX}^ϕ and chose the value of $\beta_{MX}^{(2)} = 2.0$ which was proposed by Pitzer and Mayorga (3).

The third virial coefficients, C_{MX}^ϕ , which account for ion triplet interactions, are usually very small and sometimes negligible. Therefore C_{MX}^ϕ is omitted in cases where the experimental data exist only in the range below 1.0 *m*.

In some cases these coefficients, C_{MX}^ϕ , are negative, suggesting some tendency toward ion-pair formation (2). This trend appeared in most aqueous rare earth electrolyte solutions at 25 °C.

For the cases of aqueous solutions of rare earth chlorides, nitrates, and perchlorates, the importance of differences in the parameters $\beta_{MX}^{(1)}$ was already considered by Pitzer and colleagues (24). Thus, in this calculations, we used the values of

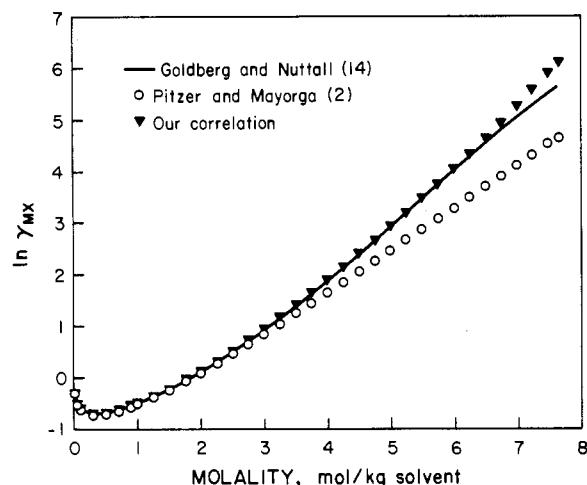


Figure 3. Comparison of experimental smoothed γ_{MX} with values calculated from Pitzer and present work for CaBr_2 at 25°C .

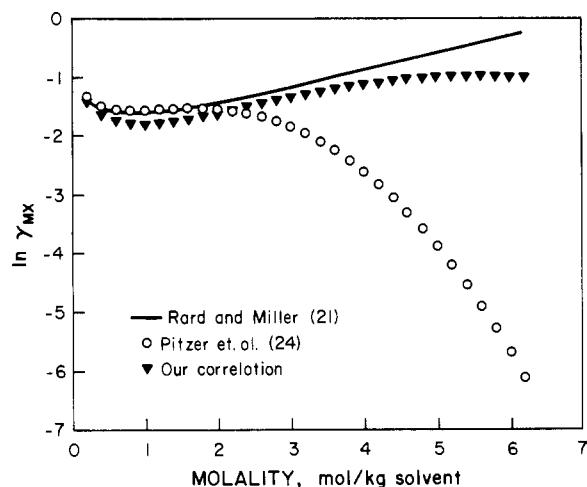


Figure 4. Comparison of experimental smoothed γ_{MX} with values calculated from Pitzer and present work for $\text{Pr}(\text{NO}_3)_3$ at 25°C .

7.7, 8.4, and 9.8 for $(3/2)\beta_{MX}^{(1)}$ for nitrates, chlorides, and perchlorates, respectively, following Pitzer et al. (24).

Comparison with Previously Published Ion Interaction Parameters

The ion interaction parameters for various single electrolytes were evaluated by a multiple regression method. The maximum molality fitted by our evaluation was the saturation concentration when data for saturated solutions were available. The standard deviations in fitting the osmotic coefficient for many salts, for instance, HCl, LiBr, CaBr_2 , and $\text{Pr}(\text{NO}_3)_3$, seem larger than Pitzer's result (2). It is important to recognize, however, that the maximum molalities for these salts are beyond those of Pitzer's evaluation.

The calculated mean activity coefficients for various single electrolytes from our results are shown in Figures 1–5 to give good agreement with available smoothed experimental data at high concentration. For example, the activity coefficient of HCl can be predicted with a standard deviation of 0.0285 in $\ln(\gamma_{\text{HCl}})$ over the entire concentration range up to 16.0 m in the experimental smoothed data by using our evaluation parameters in Table I. However, using Pitzer's values (2) for this salt, we obtain a standard deviation of 0.220 when the maximum molality is 16.0. These results are given in Table VII. Also Figure 1 shows the comparison of experimental smoothed mean activity coefficients of HCl as $\ln(\gamma_{\text{HCl}})$ with values calculated from

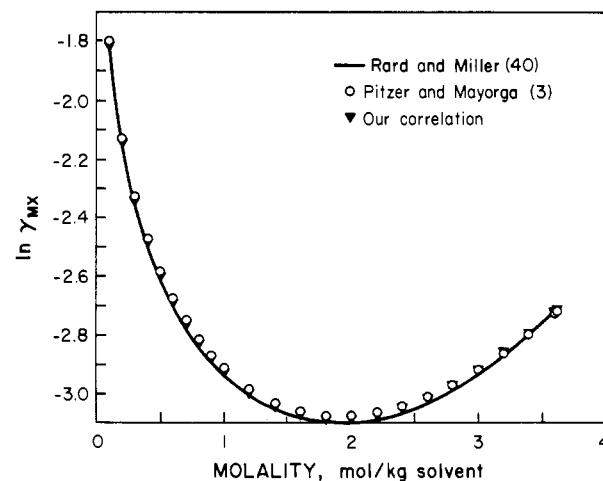


Figure 5. Comparison of experimental smoothed γ_{MX} with values calculated from Pitzer and present work for MgSO_4 at 25°C .

Table VII. Comparison of Standard Deviations for Estimated versus Experimental Activity Coefficients in Figures 1–5

salt	max molality	stand dev ^a
HCl	16.00	0.02854 (0.22031)
	6.00	0.02956 (0.00311)
LiBr	20.00	0.07224 (0.060991)
	2.50	0.06780 (0.00286)
CaBr_2	7.66	0.08760 (0.46557)
	2.00	0.00732 (0.00773)
$\text{Pr}(\text{NO}_3)_3$	6.20	0.17827 (1.78436)
	1.10	0.07117 (0.00623)
MgSO_4	3.62	0.00574 (0.00794)
	3.00	0.00385 (0.00317)

^aStandard deviations in parentheses are for salts using Pitzer's ion interaction parameter values (2) which were obtained from data up to the lower concentration given in the table for each compound. The other standard deviations are based on our evaluation of ion interaction parameters from data up to the higher concentrations reported here.

Pitzer and our work. It should be noted that the fit at lower concentrations is better using the ion interaction parameters reported by Pitzer. His parameters were obtained over a more limited range of concentration (0–6 m) than ours were.

Similar results are observed in all of the cases for which the maximum molalities go beyond that of Pitzer's evaluation. That is, Pitzer's fit gives accurate results at low concentration but poor agreements with experimental data at high concentration.

Figures 2–5 are the same kind of comparison plots of $\ln(\gamma_{MX})$ as a function of the molality for LiBr, CaBr_2 , $\text{Pr}(\text{NO}_3)_3$, and MgSO_4 . In all of these comparisons, the parameters we evaluated using data at higher concentrations give us good or better fit to the experimental data over the entire concentration range than do Pitzer's parameters. Pitzer's parameters give a better fit over the more limited range of concentrations for which parameter values were obtained, however. Standard deviations for the estimated versus experimental activity coefficients in Figures 1–5 (as $\ln \gamma_{MX}$) and the maximum concentrations corresponding to Pitzer's and our ion interaction parameter evaluations are given in Table VII.

Ternary ion interaction parameters for various mixture with common ion will be evaluated in a subsequent paper.

Literature Cited

- (1) Pitzer, K. S. *J. Phys. Chem.* 1973, 77, 268.
- (2) Pitzer, K. S.; Mayorga, G. J. *Phys. Chem.* 1973, 77, 2300.
- (3) Pitzer, K. S.; Mayorga, G. J. *Solution Chem.* 1974, 3, 539.
- (4) Pitzer, K. S.; Kim, J. J. *J. Am. Chem. Soc.* 1974, 96, 5701.
- (5) Harvie, C. E.; Weare, J. H. *Geochim. Cosmochim. Acta* 1980, 44, 981.
- (6) Harvie, C. E.; Eugster, H. P.; Weare, J. H. *Geochim. Cosmochim. Acta* 1982, 46, 1603.
- (7) Harvie, C. E.; Moller, N.; Weare, J. H. *Geochim. Cosmochim. Acta* 1984, 48, 723.
- (8) Kelly, B.; Frederick, W. J., Jr. In *Application of Chemical Engineering Principle in the Forest Products and Related Industries*; Kayihan, F., Krieger-Brackett, B., Eds.; AIChE Forest Products Division: Seattle, WA, 1986.
- (9) Chen, C. C.; Britt, H. I.; Boston, J. F.; Evans, L. B. *AIChE J.* 1979, 25, 820.
- (10) Whitfield, M. *Mar. Chem.* 1975, 3, 197.
- (11) Whitfield, M. *Geochim. Cosmochim. Acta* 1975, 39, 1545.
- (12) Hamer, W. J.; Wu, Y. C. *J. Phys. Chem. Ref. Data* 1972, 1, 1047.
- (13) Goldberg, R. N. *J. Phys. Chem. Ref. Data* 1981, 10, 671.
- (14) Goldberg, R. N.; Nuttall, R. L. *J. Phys. Chem. Ref. Data* 1978, 7, 263.
- (15) Goldberg, R. N.; Nuttall, R. L.; Staples, B. R. *J. Phys. Ref. Data* 1979, 8, 923.
- (16) Goldberg, R. N. *J. Phys. Chem. Ref. Data* 1979, 8, 1005.
- (17) Goldberg, R. N. *J. Phys. Chem. Ref. Data* 1981, 10, 1.
- (18) Spedding, F. H.; Weber, H. O.; Saeger, V. W.; Petheram, H. H.; Rard, J. A.; Habenschuss, A. *J. Chem. Eng. Data* 1976, 21, 341.
- (19) Rard, J. A.; Weber, H. O.; Spedding, F. H. *J. Chem. Eng. Data* 1977, 22, 187.
- (20) Rard, J. A.; Shiers, L. E.; Heiser, D. J.; Spedding, F. H. *J. Chem. Eng. Data* 1977, 22, 337.
- (21) Rard, J. A.; Miller, D. G. *J. Chem. Eng. Data* 1979, 24, 348.
- (22) Robinson, R. A.; Stokes, R. H. *Electrolyte Solutions*, 2nd ed.; Butterworths: London, 1959.
- (23) Pitzer, K. S. *J. Chem. Soc., Faraday Trans. 2* 1972, 68, 101.
- (24) Pitzer, K. S., Peterson, J. R.; Silvester, L. F. *J. Solution Chem.* 1978, 7, 45.
- (25) Staples, B. R. *J. Phys. Ref. Data* 1981, 10, 765.
- (26) Bonner, O. D. *J. Chem. Eng. Data* 1979, 24, 210.
- (27) Platford, R. A. *Can. J. Chem.* 1969, 47, 2271.
- (28) Bonner, O. D. *J. Chem. Eng. Data* 1978, 21, 498.
- (29) Kalman, E.; Schwabe, K. J. *Solution Chem.* 1979, 8, 1.
- (30) Bonner, O. D. *J. Chem. Eng. Data* 1982, 27, 62.
- (31) Macaskill, J. B.; Robinson, R. A.; Bates, R. G. *J. Chem. Eng. Data* 1977, 22, 411.
- (32) Staples, B. R. *J. Phys. Chem. Ref. Data* 1981, 10, 779.
- (33) Libus, Z.; Sadowska, T.; Trzaskowski, J. *J. Chem. Thermodyn.* 1979, 11, 1151.
- (34) Libus, Z.; Zak, E.; Sadowaska, T. *J. Chem. Thermodyn.* 1984, 16, 257.
- (35) Kangro, W.; Groeneveld, A. *Z. Phys. Chem. (Frankfurt am Main)* 1982, 32, 110.
- (36) Wynveen, R. A.; Dye, J. L.; Brubaker, C. H., Jr. *J. Am. Chem. Soc.* 1960, 82, 4441.
- (37) Bonner, O. D. *J. Chem. Thermodyn.* 1979, 11, 559.
- (38) Groves, K. O.; Dye, J. L.; Brubaker, C. H., Jr. *J. Am. Chem. Soc.* 1960, 82, 4445.
- (39) Bonner, O. D. *J. Chem. Thermodyn.* 1979, 11, 563.
- (40) Rard, J. A.; Miller, D. G. *J. Chem. Eng. Data* 1981, 26, 33.
- (41) Wu, Y. C.; Hamer, W. J. *J. Phys. Chem. Ref. Data* 1980, 9, 513.

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Densities and Viscosities of Binary Liquid Mixtures Containing Bromoform at 45 °C

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Densities and viscosities of eight binary liquid mixtures of bromoform with carbon tetrachloride, dimethyl sulfoxide, cyclohexane, bromobenzene, dimethylformamide, methyl ethyl ketone, ethyl acetate, and methanol are presented at 45 °C as a function of composition of the mixtures. A theoretical correlation is attempted with McAllister, Heric, and Auslander viscosity models.

Introduction

In the course of our studies on the thermodynamic properties of binary mixtures, we have reported at 25 °C excess volumes (1) and viscosities (2) for binary mixtures of bromoform with carbon tetrachloride, dimethyl sulfoxide, cyclohexane, bromobenzene, dimethylformamide, methyl ethyl ketone, ethyl acetate, and methanol. As an extension of that work, we have now measured the densities and viscosities for the same eight systems at 45 °C.

Experimental Section

All the chemicals used were of reagent grade. They were distilled by fractionating through a 2-ft column. Only bromoform

Table I. Some Physical Properties of the Liquids Studied

component	boiling point, °C		viscosity, kg/(m/s)		refractive index ^a	
	measd	lit. (4)	measd	lit. (4)	measd	lit. (4)
bromoform	149.00	149.50	0.1873	0.1890	1.5950	1.5956
carbon tetrachloride	76.20	76.75	0.0892	0.0902	1.4571	1.4574
dimethyl sulfoxide	190.00	189.85	0.2024	0.2021	1.4777	1.4773
cyclohexane	80.10	80.74	0.0883	0.0886	1.4229	1.4235
bromobenzene	155.90	156.05	0.1081	0.1040	1.5580	1.5571
dimethylformamide	152.80	153.00	0.0805	0.0800	1.4278	1.4282
methyl ethyl ketone	79.00	79.60	0.0475	0.0480	1.3759	1.3764
ethyl acetate	77.10	77.26	0.0439	0.0424	1.3702	1.3698
methanol	64.20	65.15	0.0590	0.0547	1.3258	1.3265

^aRefractive index was measured with a Abbe refractometer.

(Merck) was used directly without further purification since it was available in the highest commercial purity. Purity of the solvents was ascertained by the constancy of their boiling points during final distillations. Due to the nonavailability of direct experimental data at 45 °C for most of the solvents used here, the boiling points, viscosities, and refractive indices of the pure components at 25 °C were checked against the literature values (see Table I) to ascertain their purities (4).